WO 2004/054945 PCT/GB2003/004993

Claims

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1. A process for the production of olefins from a hydrocarbon said process comprising the steps of:

- a) passing a first feed stream comprising gaseous reactants to a first reaction zone wherein said gaseous reactants react exothermically to provide a product stream
- b) producing a mixed feed stream comprising oxygen by passing the product stream produced in step (a) and a second feed stream comprising a hydrocarbon feedstock to a mixing zone and wherein oxygen is passed to the mixing zone via one or more of (i) the product stream produced in step (a), (ii) the second feed stream comprising a hydrocarbon feedstock and (iii) a third stream comprising an oxygen-containing gas
- c) passing the mixed feed stream directly to an essentially adiabatic second reaction zone wherein in the absence of a supported platinum group metal catalyst at least a part of the oxygen is consumed and a stream comprising olefins is produced
 - d) cooling the stream comprising olefins exiting the second reaction zone to less than 650°C within less than 150milliseconds of formation
 - and wherein the temperature of the mixed stream is at least 500°C, the mixing zone and the second reaction zone are maintained at a pressure of between 1.5-50bar and the residence time within the mixing zone is less than the autoignition delay for the mixed stream.
- 2. A process as claimed in claim 1 in which an additional feed stream comprising by hydrogen is passed to the mixing zone.
 - 3. A process as claimed in claim 1 or claim 2 in which the residence time within the mixing zone is less than 100 milliseconds.

WO 2004/054945 PCT/GB2003/004993

A process as claimed in claim 3 in which the residence time within the mixing zone is less than 5 milliseconds

- 5. A process as claimed in any one of claims 1 to 4 in which the reaction is carried out in the second reaction zone at a pressure of between 5 to 30 bara
- 5 6. A process as claimed in any one of claims 1 to 5 in which the second reaction zone contains a stabiliser and/or packing material selected from the group comprising porcelain, ceramics, alumina and silica that do not exhibit any substantial catalytic activity
- 7. A process as claimed in any one of claims 1 to 6 in which the second reactor contains an ignition source.
 - 8. A process as claimed in any one of claims 1 to 7 in which the pressure of the second reaction zone is maintained at a pressure of between 5.0-10.0bara and the products are quenched by reducing the temperature to less than 650°C within less than 50milliseconds of formation.
- 9. A process as claimed in any one of claims 1 to 7 in which the pressure of the second reaction zone is maintained at a pressure of between 10.0-20.0bara and the products are quenched by reducing the temperature to less than 650°C within 20milliseconds of formation.

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